APPENDIX 1

Copies To: J.H.E.B.
L.B.C.
A.J.D.
M.B.W. ✓

Your Ref: PET16/20/209.
Our Ref: RSE/RGS/D3/14.

15th September, 1978.

Department of Energy,
Thames House,
South Millbank,
London, SW1P.4QJ.

For the attention of the Pipeline Inspector.

Dear Sir,

Re: Local Pipe-line Parkeston Quay.

Further to our letter dated 11th August, 1977 and your letter dated 16th November, 1977 we wish to give notice, in accordance with Section 36 (1)(a) of the Pipe-lines Act 1962, that the local pipe-line which was the subject of those letters was taken into use on Friday, 8th September, 1978.

This notification covers all the pipe-line concerned consisting of 335 metres length inside existing refinery boundaries plus 615 metres between the refinery and Parkeston Quay as detailed in the Technical Specification.

We trust this information meets your requirements.

Yours faithfully,
for CARLESS SOLVENTS LIMITED.

R. S. Emerson.

R. S. EMERSON.
REFINERY MANAGER.

C.C.N.U.

Our ref: RSE/JC/D3/14

The Pipe-lines Inspector,
Room 1368,
Department of Energy,
Thames House South,
Millbank,
London SW1P 4QJ.

11th.August 1977

F.A.O. Mr.K.F.Paddock

Dear Sir,

re: Local Pipe-line Parkeston Quay

In accordance with the Pipe-lines Act, 1962, we wish to give notice of intention to construct a local pipe-line at Parkeston Quay, Essex.

Please find enclosed the proposed technical specification and map (Ordnance Survey Plan TM 2232 and TM 2332) showing the route marked in RED (broken line for underground section).

Answers to the questions raised by Section 2(2) of the Act are:-

a. The owner of the proposed pipe-line will be:-
CARLESS SOLVENTS LIMITED,
Petrol House,
Hepscott Road,
Hackney Wick,
London E.9.

b. The proposed pipe-line to run inside the existing eight foot pipe-line track between Carless Solvent's Refinery and Parkeston Quay. The proposed pipe-line is to connect into an existing loading arm at the Quay.

c. Consent to this proposal is required from:-

i. British Rail, who own the land involved.

ii. The Anglian Water Authority, as the proposed route, within the existing Refinery boundary, utilises a sea defence wall.

iii. H.M.Customs and Excise.

These appropriate 'consents' are being sought, and are expected to be obtained.

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d. It is proposed to convey Class 'A' and 'B' petroleum products. (As defined by the Petroleum (Consolidation) Act 1928).

e. See enclosed technical specification.

As required by Section 35(2) of the Pipe-lines Act, 1962 a copy of the enclosed map has been sent to the Chief Technical Officer of Tendring District Council.

We trust that the enclosed information is to your satisfaction.

Yours faithfully,
for CARLESS SOLVENTS LTD.

R.S. Emerson.

R.S.EMERSON
Refinery Manager

c.c. M.B.W.

PIPELINES ACT 1962

Pipeline System - Technical Specification

1. Design	
Steel Specification.	Stainless Type 316 Spiral or longitudinal weld.
Diameter.	219 m.m. O.D.
Nominal wall thickness and tolerances if other than A.P.I.	2.7 m.m.
Manufacturers mill test pressure.	To A.S.T.M. Standard
Total length of pipeline/system.	Outside existing Refinery 615 met Inside existing Refinery 335 met
Maximum and minimum operating temperatures.	Ambient
Maximum working pressure.	100 lb. per square inch
Test pressure to be imposed.	150 lb. per square inch
Type and rating of flanges, valves, etc.	150 lb. rating. Carbon steel valves
Type and thickness of anti-corrosion coating.	Denso wrapping:- 2 coats, under-ground sections only.
Method of interanl protection.	None
Type of cathodic protection systems and details of terminations.	None
Codes of Practice being followed.	The Institute of Petroleum Model C of Safe Practice 'Petroleum Pipel Part 6 1967.

2. Operating Data

Design throughput.	300 Metric tons per hour
Type rating and location of pumps serving the pipeline.	Centrifugal 5000 litre per minute pumps located inside Refinery
System of flow measurement and specified degree of accuracy.	Automatic storage tank gauging

3. Operational Safety

Method and frequency of inspection.	Pipe-line walked each time used. Annual pressure test.
Safety devices and locations.	Thermal relief valves situated inside Refinery.
Method of leak detection.	Pressure test and visual.
Emergency shut down system.	Manual control of valves. Telephone and portable radio communication between each end of the pipe-line.
Location of system valves.	See enclosed Drawing No.H1264